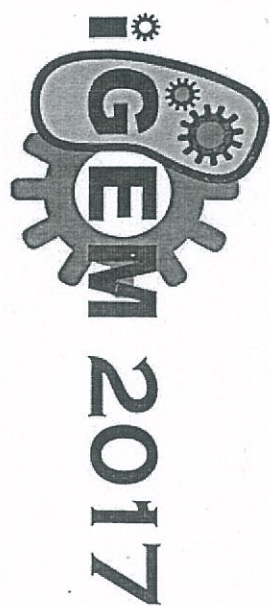


中国海洋大学“东升本科生发展基金”申请表

(2017 年)

申请人情况	姓名	陈宇卿		性别	女	民族	汉族
	学院	海洋生命学院	专业	生物技术	学号	15050031004	
	电话	17806276755			邮箱	ykkchen@outlook.com	
团队成员情况 (个人申报无需填写)	陈宇卿、15050031004、海洋生命学院、2015 级生物技术、队长 穆榕、15060021039、水产学院、2015 级水产养殖、副队长 赛务 王中石、15050011076、海洋生命学院、2015 级生物科学、副队长 曲佳乐、15050011052、海洋生命学院、2015 级生命科学、实验室管理员 陈颖、15050011010、海洋生命学院、2015 级生命科学、实验室管理员 张千夏、15050031061、海洋生命学院、2015 级生物技术、实验员 财务 田硕、15000021035、环境科学与工程学院、2015 级环境工程、干组负责人 数学建模 朱磊、15050021041、海洋生命学院、2015 级生态学、干湿协调员 实验员 闫舒恒、15060021078、水产学院、2015 级水产养殖学、美工网页制作 实验员 丁喜仲、15070031005、食品科学与工程学院、2015 级海洋资源开发技术、实验员 范云昊、15050031007、海洋生命学院、2015 级生物技术、实验员 胡舒楠、15050031016、海洋生命学院、2015 级生物技术、实验员						
竞赛整体情况	国际基因工程机器大赛, International Genetically Engineered Machine competition, 简称 iGEM。是合成生物学领域的国际顶级大学生科技赛事, 也是涉及数学、计算机、统计学等领域交叉合作的跨学科竞赛。由美国麻省理工学院于 2003 年创办, 2005 年发展成为国际赛事, 于每年 10、11 月在麻省理工学院进行最终角逐。iGEM 竞赛本次参赛队伍全世界共 313 支, 立陶宛维尔纽斯大学 Vilnius-Lithuania 获得了总冠军 Grand Prize Winner, 美国威廉玛丽学院 William and Mary 获得亚军 1st Runner Up, 德国海德堡大学 Heidelberg 获得季军 2nd Runner Up。中国地区共有 98 支 iGEM 团队参赛 (含退赛), 包括中国大陆地区 83 支, 香港特区 5 支, 台湾地区 10 支。与 2016 年相比, 大陆地区增加了 20 支队伍, 增幅惊人, 也远远高于全球参赛队伍数量的增长率, 比赛规则较往年更加严格。中国地区, 共有 79 支队伍 (含港台地区) 获得了奖牌, 其中大陆地区 66 支, 香港特区 4 支, 台湾地区 9 支。中国大陆地区的 83 支团队中, 有 12 支得到了单项奖或单项提名奖。我团队位列其中, 与北京大学等高校齐名。Best New Basic Part 的筛选来自于全球 313 支队伍提交的近 3000 个标准化的基因元件中, 全球获得此奖项的队伍共 8 支。						
当年获奖情况	(1) 获国际金奖 (2) 【单项奖】Nominated Best New Basic Part 奖: 中国大陆地区的 83 支团队中, 有 12 支得到了单项奖或单项提名奖。我团队位列其中。Best New Basic Part 的筛选来自于全球 313 支队伍提交的近 3000 个标准化的基因元件中, 全球获得此奖项的队伍共 8 支。				申请额度 (万元)	5 万元	
参赛费用支出情况 获得经费支持及	项目类型	具体内容				支出金额 (元)	
	实验经费	试剂购买、基因合成、引物合成、测序等				45750.5 (海洋生命学院获得补助 35000 元, 校外赞助 10000 元)	
	参赛经费	队伍注册费、jamboree 门票 (6 张)				55807.53 (暂未获得补助)	
	国际差旅	12 名队员国际差旅及住宿费用				71612.9 (暂未获得补助)	
	国内差旅	与国内其他高校 (北京大学、福建农林大学) 交流、与山东大学、北京化工大学教授交流, 参加上海合成生物学学者论坛				25575 (暂未获得补助)	
	日常花费	签证办理及日常打印、队服等				14700 (暂未获得补助)	
指导教师意见	 指导教师 (签字) 年 月 日			学院审核	 分管教学副院长 (签章) 年 月 日		
管委会意见							

1. 竞赛介绍包括竞赛主办方、比赛内容、参赛队伍数量、奖项设置及竞赛影响力等;
2. 获得经费支持情况包括学校支持经费额度、学院支持经费额度、教师科研经费支持额度及其他经费支持; 参赛费用支出情况包括出境参赛人数、国际差旅费支出、国内差旅费支出、实验材料支出及其他费用支出;
3. 中国海洋大学“东升本科生发展基金”管理委员会办公室制表。



INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

YUQING CHEN

OUC-CHINA



GIANT JAMBOREE

NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



由 扫描全能王 扫描创建



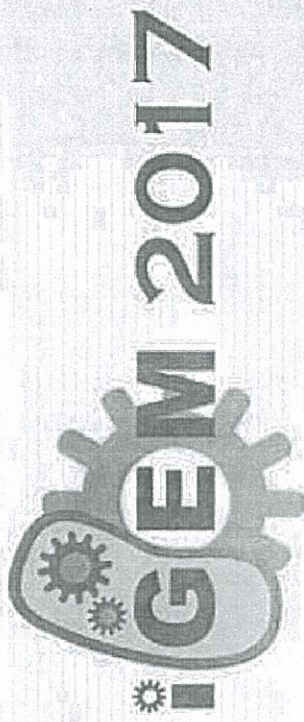
INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

TIAN SHUO

OUC-CHINA



GIANT JAMBOREE
NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

RONG MU

OUC-CHINA



GIANT JAMBOREE
NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

XIZHONG DING

OUC-CHINA



GIANT JAMBOREE
NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

LEI ZHU

OUC-CHINA



GIANT JAMBOREE
NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



IGEM 2017

INTERNATIONAL GENETICALLY ENGINEERED MACHINE COMPETITION

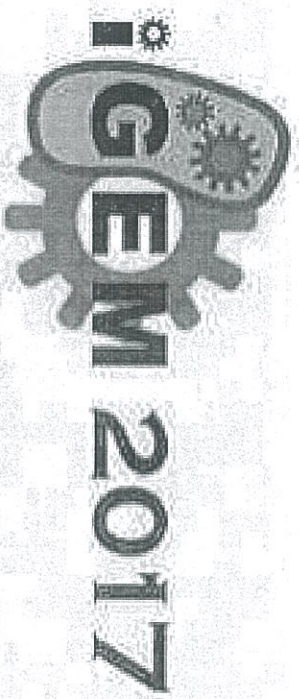
JIALE QU

OUC-CHINA



GIANT JAMBOREE

NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

ZHONGSHI WANG

OUC-CHINA

GIANT JAMBOREE

NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS





INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

YUNHAO FAN

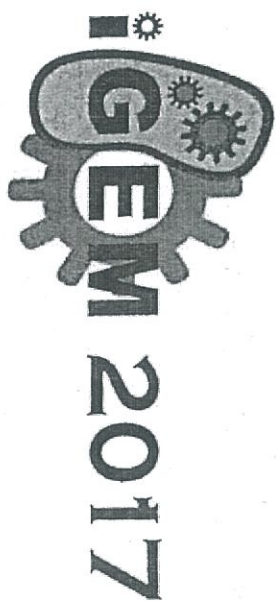
OUC-CHINA



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INTERNATIONAL GENETICALLY ENGINEERED MACHINE
COMPETITION

CHEN YING

OUC-CHINA

GIANT JAMBOREE
NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS



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GIANT JAMBOREE

NOVEMBER 9 - NOVEMBER 13, 2017



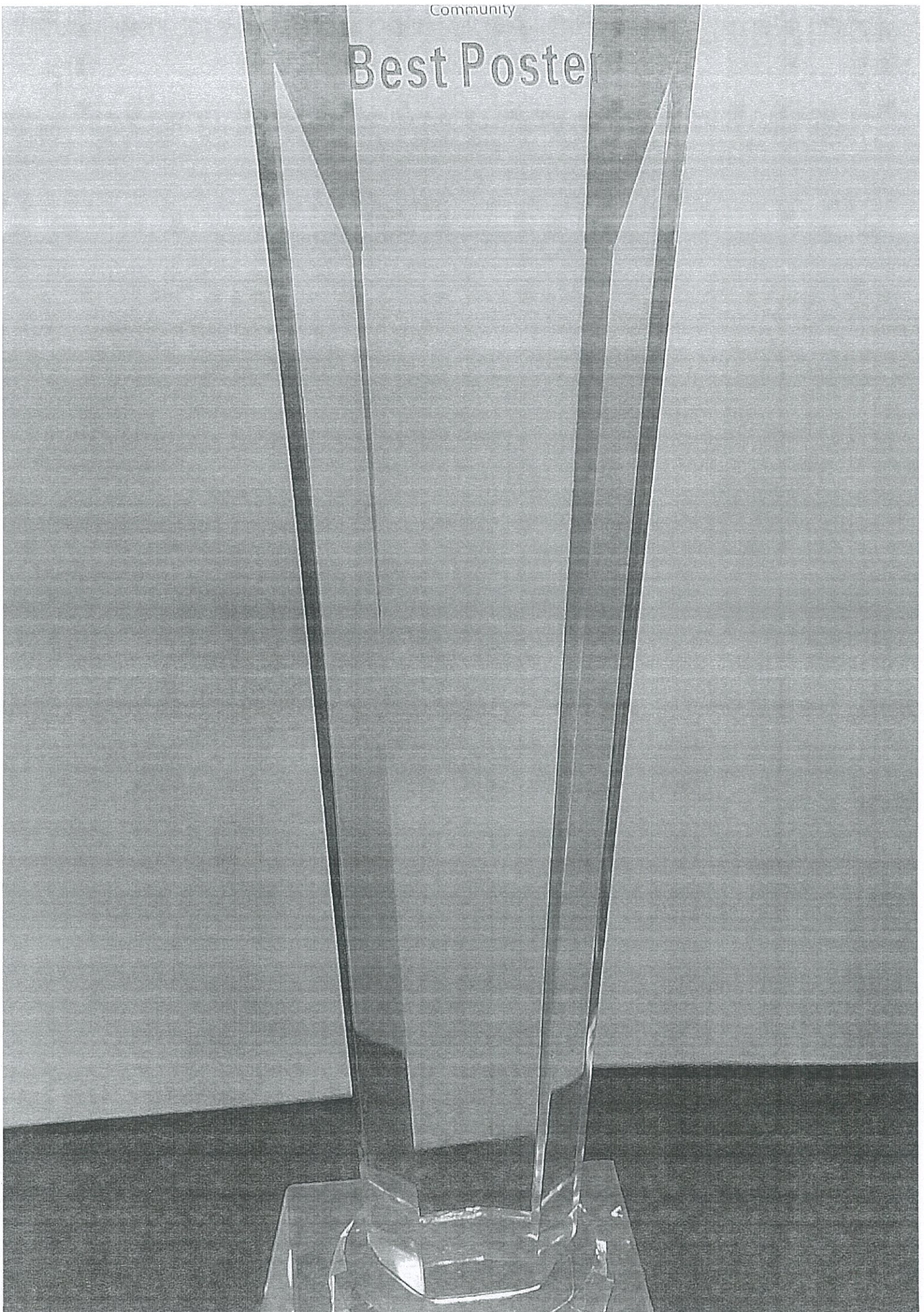
QIANXIA ZHANG



GIANT JAMBOREE
NOVEMBER 9 - NOVEMBER 13, 2017
BOSTON, MASSACHUSETTS

Community

Best Poster

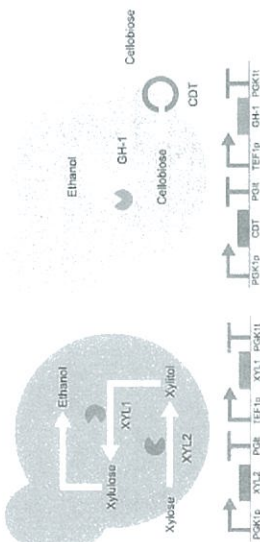




Ethanol from Algae

Turning algal bloom into clean energy

In regard of glucose repression, we ferment xylose & cellobiose from pretreated *Enteromorpha* powder with two separated *S. cerevisiae* strains, so that the intracellular hydrolysis of cellobiose minimizes glucose repression of xylose fermentation. For yeast A, we introduced cellobiose transporter and β -glucosidase genes, and in yeast B we expressed xylool dehydrogenase and xylose reductase. These two strains that can live on either cellobiose or xylose and produce ethanol through their own metabolic pathways, which means they can ferment cellobiose and xylose synergistically. It will be a big step further since the yeast can take the place of chemicals and fulfill this meaningful task.



We ferment xylose & cellobiose from pretreatment of *Enteromorpha* powder with two recombinant *S. cerevisiae* strains we constructed. Compared to wild type yeast, they can live happily on xylose & cellobiose as sole carbon source. We characterized their ability by measuring (i) the amount of biomass, (ii) the concentration of xylose or cellobiose, (iii) the production of ethanol over time with plate reader, HPLC or SBA.

Adhesion platform

Engineering *E. coli* the surface-display system of yeast for more potential

When dealing with cellulose decomposition, it is natural to think of cellulose, which functions as a surface-display scaffold and helps express relevant enzymes. However, the advantages of synergistic effect and proximity effect are largely limited by its complicated structure, which leads to a huge metabolic burden. By adhering *E. coli* to *S. cerevisiae*, this substituted 'surface-display system' can reserve these advantages as well as broaden the potential functions of the yeast as a model organism rather than a scaffold.

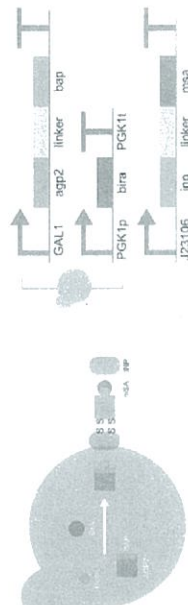


Fig 1: The sketch of adhesion platform.

Validation of Protein Expression

Proof 1

> In *E. coli*

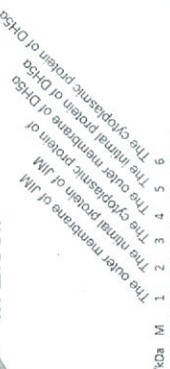


Fig 2: The sketch of adhesion platform.

Validation of Protein Function

Proof 2

Co-existence of *E. coli* and *S. cerevisiae* even after rinsing--ADHESION VALIDATION!



Fig 3: The result of confocal laser scanning microscopy

Model

The aim to the adhesion platform is binding the *E. coli* to *S. cerevisiae*

Qualitative Validation

Proof 1



Quantitative Validation

Proof 2

- Increase in ethanol
- Increase in biomass
- Decrease in xylose & cellobiose

> XYLOSE

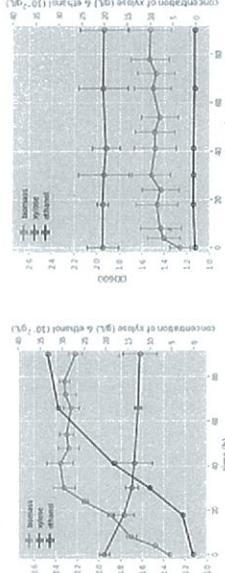


Fig 1.1 Concentration change of xylose, ethanol and biomass (n=4) of engineered strain with xylose-utilizing circuit

> CELLOBIOSE

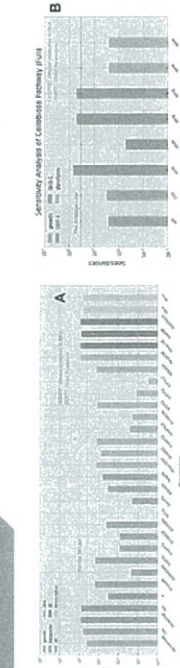


Fig 1.2 Concentration change of xylose, ethanol and biomass (n=4) of WT strain

Model

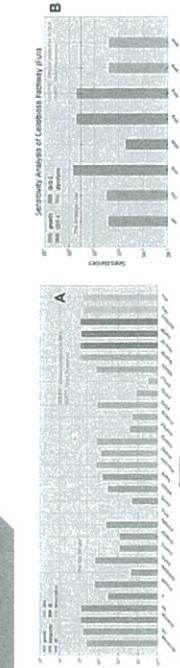


Fig 2.1 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

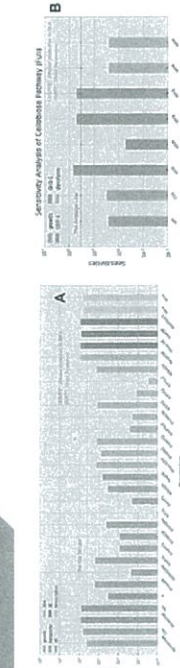


Fig 2.2 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

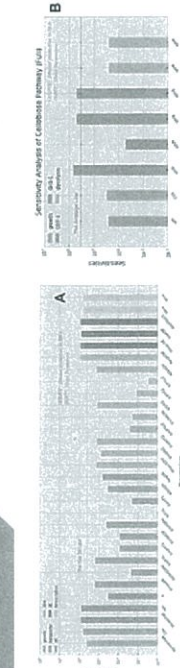


Fig 2.3 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

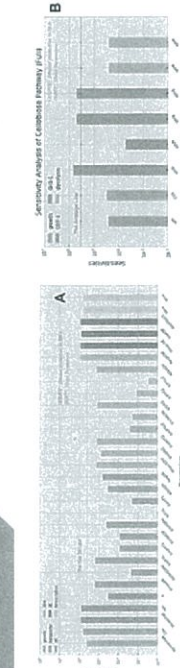


Fig 2.4 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

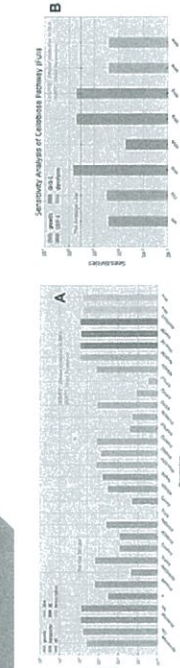


Fig 2.5 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

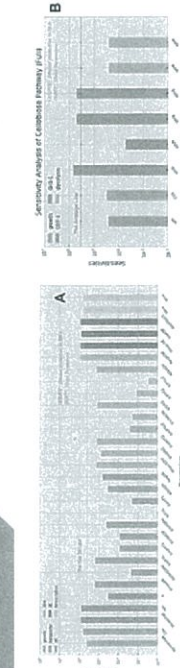


Fig 2.6 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

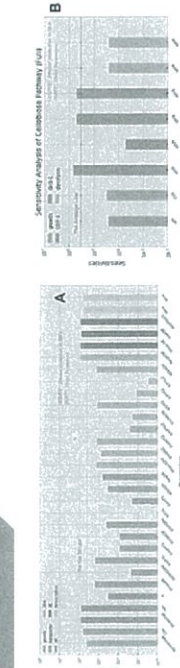


Fig 2.7 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

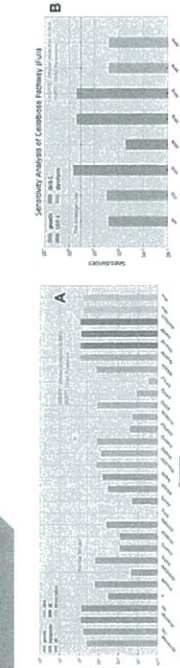


Fig 2.8 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

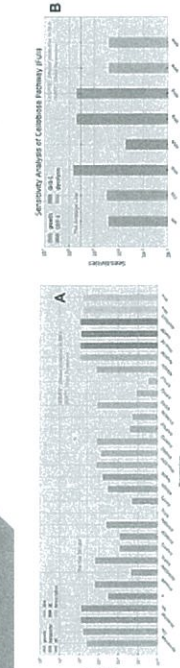


Fig 2.9 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

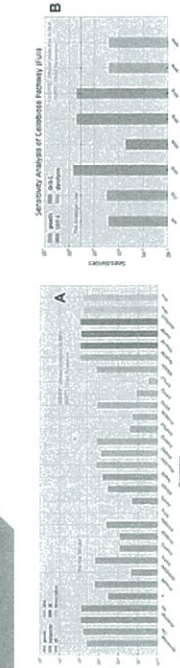


Fig 2.10 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

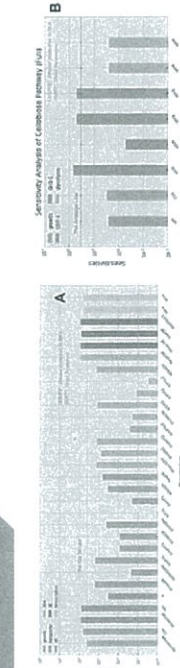


Fig 2.11 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

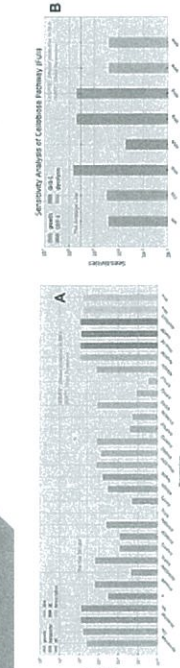


Fig 2.12 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

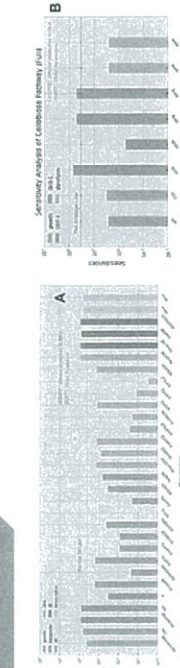


Fig 2.13 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

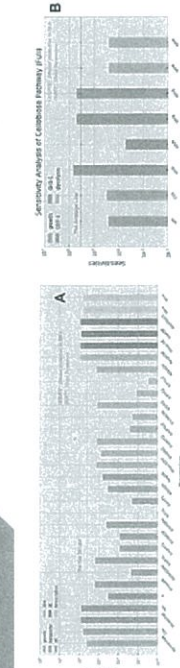


Fig 2.14 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

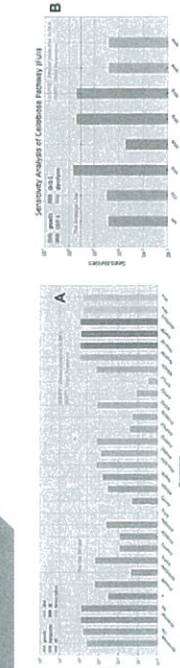


Fig 2.15 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

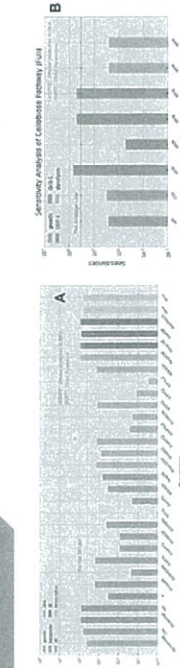


Fig 2.16 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

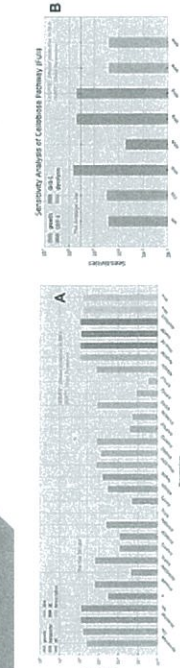


Fig 2.17 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

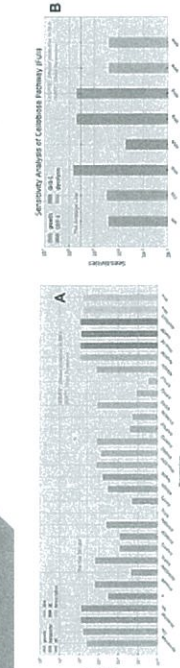


Fig 2.18 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

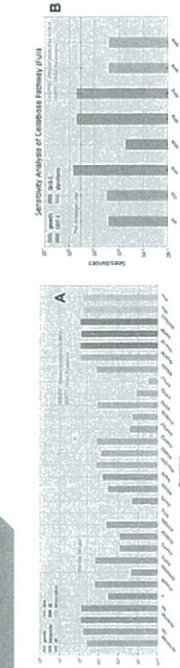


Fig 2.19 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

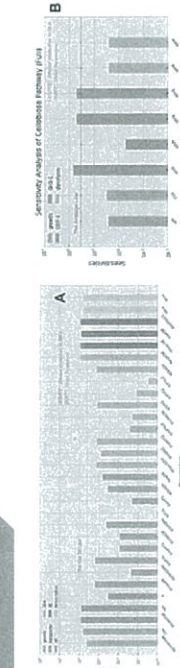


Fig 2.20 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

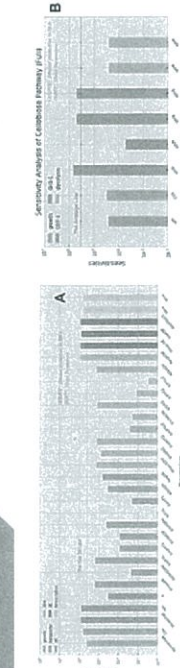


Fig 2.21 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

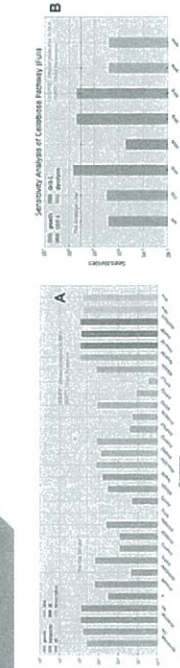


Fig 2.22 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

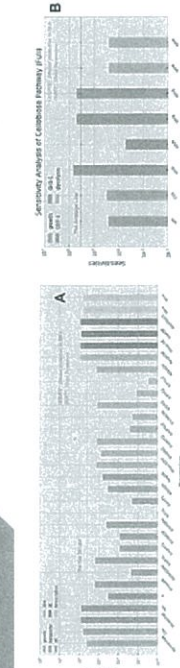


Fig 2.23 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

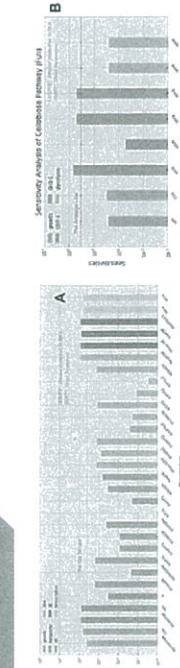


Fig 2.24 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

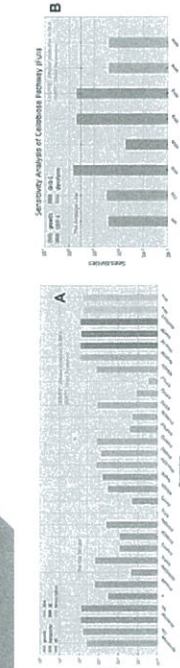


Fig 2.25 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

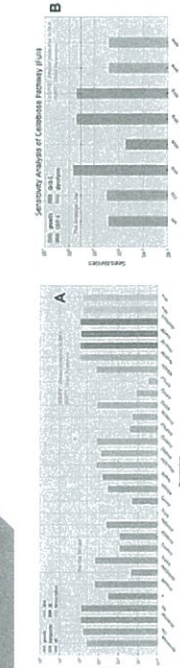


Fig 2.26 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

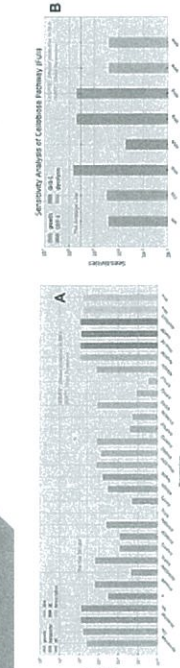


Fig 2.27 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

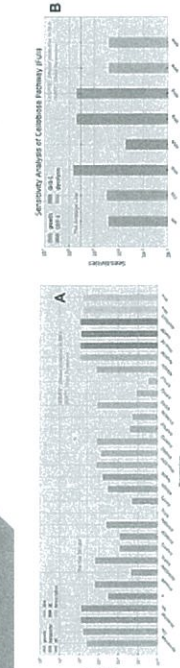


Fig 2.28 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

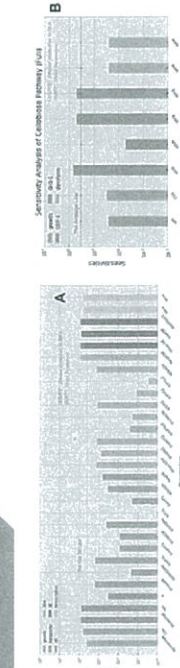


Fig 2.29 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

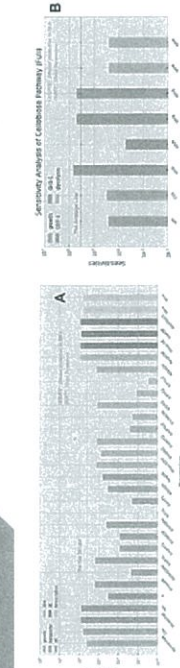


Fig 2.30 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

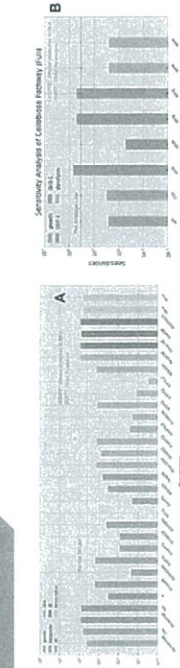


Fig 2.31 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

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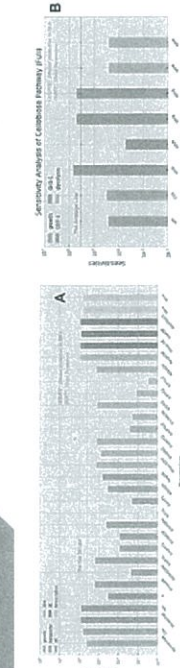


Fig 2.32 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

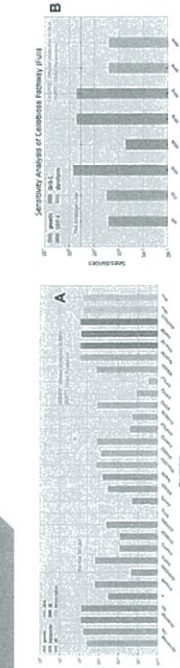


Fig 2.33 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

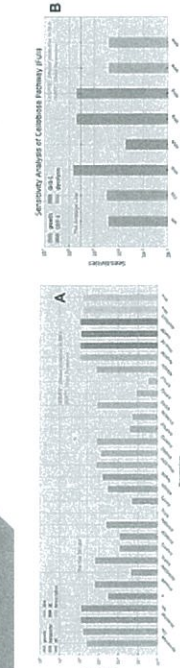


Fig 2.34 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

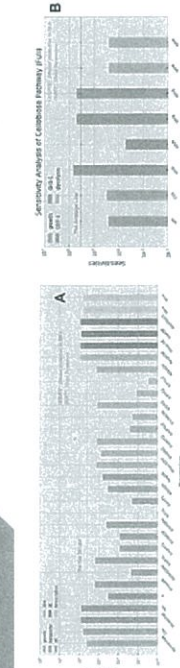


Fig 2.35 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

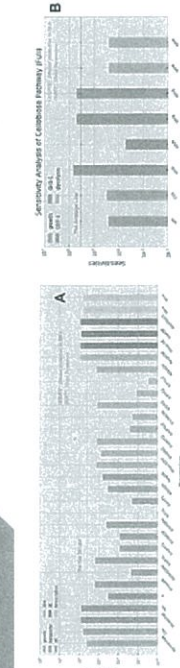


Fig 2.36 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

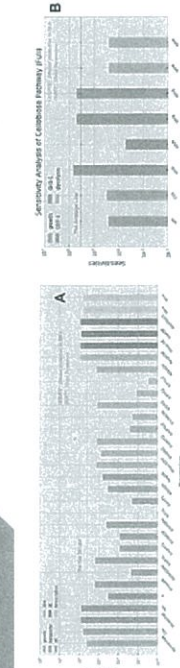


Fig 2.37 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

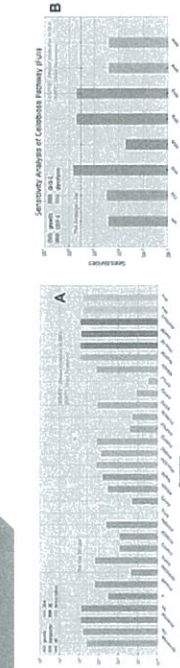


Fig 2.38 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

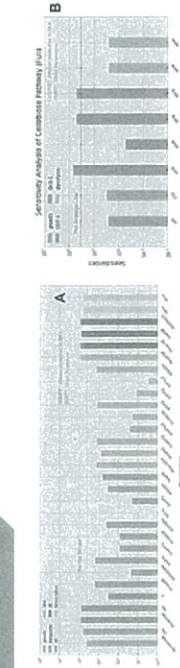


Fig 2.39 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

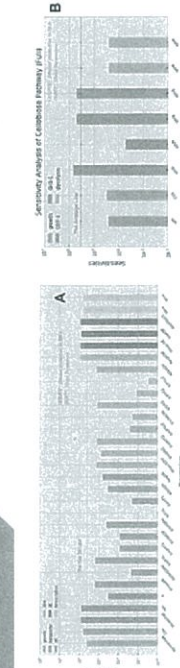


Fig 2.40 Concentration change of cellobiose, ethanol and biomass (n=4) of WT strain

Model

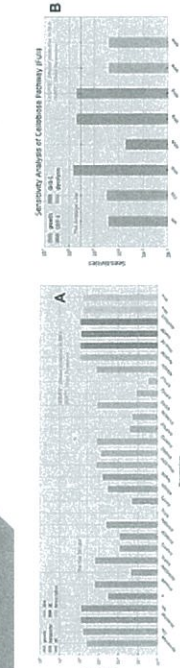


Fig 2.41 Concentration change of cellobiose, ethanol and biomass (n=4) of engineered strain with cellobiose-utilization circuit.

Model

